## Steam Reforming of the Olive Mill Wastewater in Multifunctional Reactors

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Olive oil production is one of the agro-industrial sectors with major critical environmental impacts: the olive oil mill wastewater (OMW) is a pollutant by-product of this process [1]. In this way, it was suggested the application of the OMW steam reforming (OMWSR), which can economically valorize this waste (H<sub>2</sub> production). A hybrid reactor configuration combining the OMWSR with H<sub>2</sub> and CO<sub>2</sub> selective removal is proposed herein for the 1<sup>st</sup> time, due to its potential to overcome the restrictions of the reversible reactions. It was compared the performance of a traditional reactor (TR), a sorption-enhanced reactor (SER - with CO<sub>2</sub> sorbent), a membrane reactor (MR - with an H<sub>2</sub>-selective membrane) and the sorption-enhanced membrane reactor (SEMR - integrating both separations).

The best operating conditions for the OMWSR in a SEMR were determined in a thermodynamics analysis [2]. The H<sub>2</sub> yield increases with the H<sub>2</sub> and/or CO<sub>2</sub> removal. It was also verified that the advantages of the SEMR are more perceptible at lower temperatures, and so this reactor configuration can be operated under milder conditions, which favor CO<sub>2</sub> sorption and membrane stability. Among the prepared hydrotalcites, the one modified with gallium and with potassium, presents the highest CO<sub>2</sub> sorption capacity in comparison with the other synthesized and even commercial sorbents [3]. About the catalysts screening, the Rh-based, as well as the Ni/SiO<sub>2</sub>-Al<sub>2</sub>O and Ni-Ru/SiO<sub>2</sub> samples, reached the highest values of H<sub>2</sub> yield. Among them, the Rh/Al<sub>2</sub>O<sub>3</sub> and Ni/SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> catalysts presented a high and stable H<sub>2</sub> yield during 24 h of time-on-stream [4].

The removal of H<sub>2</sub> and CO<sub>2</sub> allowed reaching higher and stable H<sub>2</sub> yields in the SEMR during the pre- and pos-breakthrough time in comparison with the TR (see Fig. 1a-b)) [5]. This allows the simultaneous production of highly pure H<sub>2</sub> in the retentate and permeate sides. A higher improvement in terms of H<sub>2</sub> yield was observed when the MR and particularly the SEMR was applied (see Fig. 1c) - H<sub>2</sub> yield enhancement of  $\approx$  44 % was noted compared to the TR). It was also demonstrated that the steam reforming process, when implemented in a SEMR, can efficiently handle real OMW effluents, with high productions of H<sub>2</sub>.

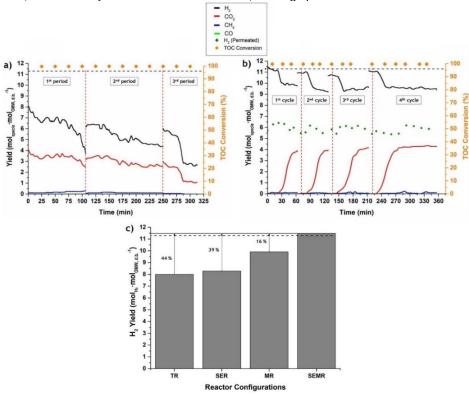


Fig. 1. Gaseous species yield and TOC conversion in a) TR or b) SEMR at 400 °C/4 bar. c) H<sub>2</sub> yield with different reactor configurations at 400 °C/4 bar.

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